

*Dedicated to Prof. Dr. H. J. Seifert on the occasion of his 60<sup>th</sup> birthday*

## **INVESTIGATION OF THE PHASE BAROGRAMS AND DIAGRAMS OF THE GeI<sub>4</sub>-I<sub>2</sub>, GeI<sub>4</sub>-BiI<sub>3</sub> AND GeI<sub>4</sub>-HgI<sub>2</sub> SYSTEMS**

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The phase barograms of the systems GeI<sub>4</sub>-I<sub>2</sub>, GeI<sub>4</sub>-BiI<sub>3</sub> and GeI<sub>4</sub>-HgI<sub>2</sub> were determined by total pressure measurements in a membrane zero manometer and the resulting phase diagrams were compared with those obtained by DTA measurements. All the systems were single eutectics.

In previous works, the HgI<sub>2</sub>-I<sub>2</sub> [1, 2] and the BiI<sub>3</sub>-I<sub>2</sub> and BiI<sub>3</sub>-HgI<sub>2</sub> [3] phase systems were investigated, and it was stated that the single eutectic systems are very similar, they have nearly ideal melting behaviour and their barograms are of similar structure. We carried on by investigating the GeI<sub>4</sub>-I<sub>2</sub>, GeI<sub>4</sub>-HgI<sub>2</sub> and GeI<sub>4</sub>-BiI<sub>3</sub> systems, among them the melting diagram for GeI<sub>4</sub>-I<sub>2</sub> is known [4] and, concerning the two others, a single eutectic nature was expected due to the similar molecular structure.

The melting diagram of all three systems were calculated assuming ideal solution behaviour following Raoult's law

$$\log N_A = - \frac{\Delta H_L}{2.303 \cdot R} \left( \frac{T_0 - T}{T_0 \cdot T} \right)$$

where the temperature dependence of the heat of melting  $\Delta H_L$  with  $C_p(T - T_0)$  was taken into account and

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$$\log N_A = - \left( \frac{\Delta H_L - C_p \cdot T_0}{2.303 \cdot R} \right) \left( \frac{T_0 - T}{T_0 \cdot T} \right) + \frac{\Delta C_p}{R} \cdot \log \left( \frac{T}{T_0} \right)$$

was obtained [1, 2], where  $N_A$  is the molar fraction of the substance  $A$ ,  $\Delta H_L$  the heat of melting,  $\Delta C_p$  is the molar heat difference,  $R$  the gas constant,  $T_0$  the melting temperature of the substance  $A$ , and  $T$  the melting temperature of the system with a molar fraction of  $N_A$ .

$\text{GeI}_4$ ,  $\text{BiI}_3$  and  $\text{GeI}_2$  were obtained by direct synthesis from the elements in a closed tube and a two zone furnace ( $\text{GeI}_4$ :  $750^\circ \rightarrow 180^\circ$ ;  $\text{BiI}_3$ :  $450^\circ \rightarrow 180^\circ$ ;  $\text{HgI}_2$ :  $225^\circ \rightarrow 180^\circ$ ) and purified by subsequent sublimation.  $\text{I}_2$  was simply resublimated. The substances were stored and put into the membrane zero manometer in small quartz glass ampoules with a bottom drawn towards the interior [2].

## 1. The $\text{GeI}_4$ - $\text{I}_2$ system

### 1.1 Total pressure measurements, barogram

From previous investigations of the  $\text{Ge}-\text{I}_2$  [5] system, the phase diagram of the total system  $\text{Ge}-\text{I}_2$  on the side rich in  $\text{Ge}$  was deducible, i. e. in the  $\text{Ge}-\text{GeI}_2$  and  $\text{GeI}_2-\text{GeI}_4$  sections, the phase barogram of the  $\text{GeI}_4-\text{I}_2$  was unknown. The total pressure curves in relation to liquid  $\text{GeI}_4$  have been determined repeatedly [5–7], the evaporation curve of iodine is well known; compare [2, 3 and 8].

To measure the total pressure of  $\text{GeI}_4-\text{I}_2$  mixtures, different  $\text{GeI}_4/\text{I}_2$  ratios were used so that the total saturation curve along the monovariant three-phase line was ensured to be solid-liquid-gaseous, along the monovariant two-phase lines solid-gaseous and liquid-gaseous, respectively, for the  $\text{GeI}_4$  and  $\text{I}_2$  boundary phases.

In Fig. 1, the measured pressure-temperature composition data were registered, the result being the phase barogram of the  $\text{GeI}_4-\text{I}_2$  system.

The total pressure curve of iodine goes up to the melting point  $S_1$  at  $114^\circ$  along the logarithmic  $1/T$  straight line (1) and is consistent with previous measurements [2, 3]. At the melting point,  $146^\circ$ , the vapour pressure is about 3.5 torr and, with regard to its course the curve best corresponds to the measurements of Chernyaev *et al.* [6]. Mixing on the eutectic side rich in  $\text{I}_2$  – see Fig. 2. – a total pressure course is shown along the  $\text{I}_2$  straight line up to nearly above  $100^\circ$  (and afterwards bends, curve 2). At the bending

point, the precipitates contain 10 mol% GeI<sub>4</sub>. In the case of mixtures, which have a greater GeI<sub>4</sub> content than in consistency with the eutectic, the curves bend at *E* from the total saturation curve of iodine, pass a pressure maximum and approach the GeI<sub>4</sub> saturation vapour pressure at *S*<sub>2</sub>. At about 130°, the maximum pressure value of the *E*-*S*<sub>2</sub> three-phase line is 35 torr. Because of the low iodine content of samples 6 and 8, the pressure curve does not completely pass the three-phase line, but it deviates from the saturation curve and until meeting it again goes on at higher temperature with a smaller slope. For samples 3-8 the bending points from the three-phase line correspond to the melting temperatures of the really existing

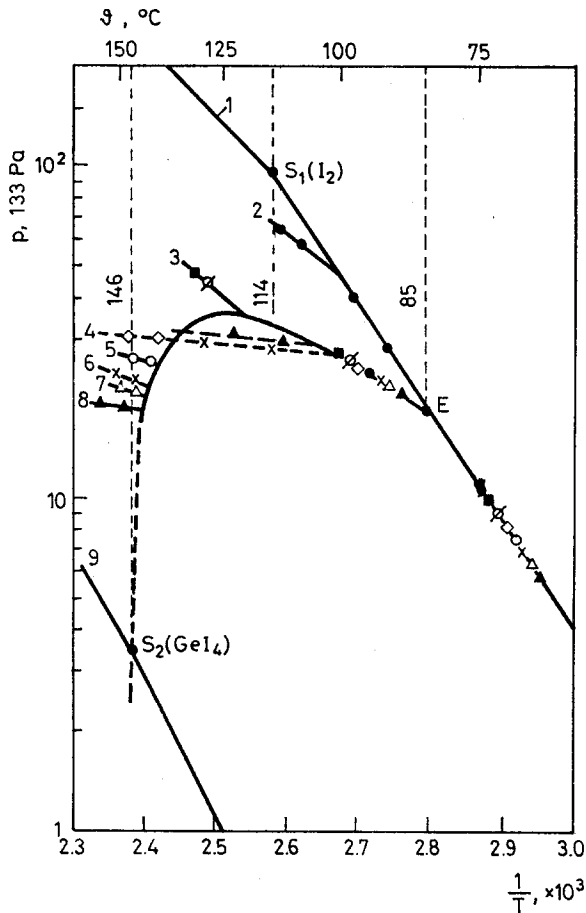


Fig. 1 Phase diagram of GeI<sub>4</sub> - I<sub>2</sub> system Mole per cent: 1 - I<sub>2</sub>; 2 - 10; 3 - 60; 4/5 - 88; 6 - 90; 7 - 92.8; 8 - 93; 9 - GeI<sub>4</sub>

precipitate compositions indicated in Fig. 1 (description of the figure). The melting points obtained are registered in Fig. 2.

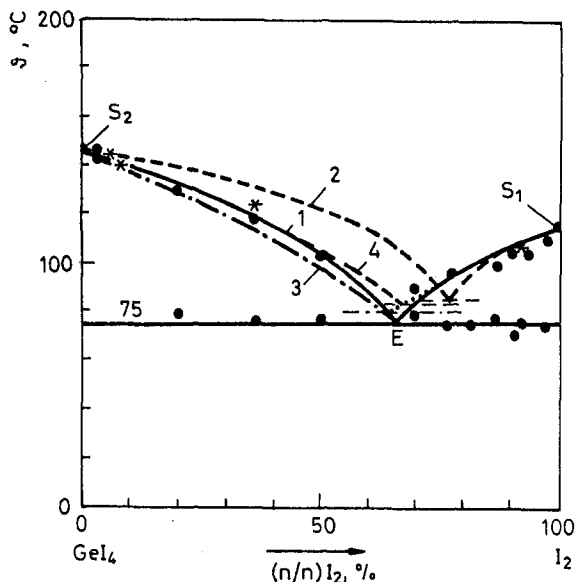


Fig. 2 Melting diagram for the GeI<sub>4</sub>-I<sub>2</sub> system; 1 - DTA curve; 2 - Maneglier *et al.* [4]; 3, 4 - calculated with  $\Delta H_L = 4.61$  kcal/mol or 5.35 kcal/mol \* - from total pressure measurements, Fig. 1

It is remarkable that during the cooling process the course of three-phase line cannot be explained in spite of the long temperature holding times. At low temperatures, only pressures along the saturation vapour pressure of iodine were measured. This phenomenon indicates a supercooled melt. When heating these mixtures again, the course along the three-phase line is observed.

Because of the comparatively low total pressure of the three-phase line, slight inaccuracies in the determination of pressure-temperature value pairs result in relatively high deviations in the melting temperature of the relevant precipitates.

### 1.2 Calculation of the GeI<sub>4</sub>-I<sub>2</sub> melting diagrams

Proceeding from the relations mentioned, the liquidus lines for the boundary phases GeI<sub>4</sub> and I<sub>2</sub> were calculated. As heat of fusion for GeI<sub>4</sub>, the value of 4.61 kcal/mol (19.3 kJ/mol) [5] and 5.35 kcal/mol (22.4 kJ/mol) [5] were applied and, for iodine 3.77 kcal/mol (15.8 kJ/mol) [10]. The melt-

ing temperatures are  $146^{\circ}$  (419 K) for  $\text{GeI}_4$  and  $114^{\circ}$  (387 K) for iodine. The medium molar heat difference of the liquid and solid for  $\text{GeI}_4$  is  $\Delta C_p = 4.2 \text{ cal/k}\cdot\text{mol}$  ( $17.6 \text{ J/k}\cdot\text{mol}$ ) [11–13], for details see [14].

The liquidus lines for  $\text{GeI}_4$  calculated from both values of heat of fusion are indicated in Fig. 2. Accordingly, the eutectic composition should be at 36 or 32% (n/n)  $\text{GeI}_4$ . The eutectic temperature is determined as  $80^{\circ}$  (353 K) to  $85^{\circ}$  (358 K).

### 1.3 Differential thermal analysis–melting diagram

As already described [9], the differential thermal investigations were carried out using a modified DTA apparatus. DTA ampoules were made using Rasotherm glass with a thin bottom of these ampoules was drawn towards the interior of the ampoule. For the measurements, each time 100 mg of the mixture was weighed, put into the ampoule and melted in vacuo. The heating rate was 5 deg/min. In Fig. 3, as an example, the curve is shown for a mixture containing 12.7% (n/n) of  $\text{GeI}_4$  and 87.3% (n/n) of  $\text{I}_2$ . As the eutectic temperature, the intersection point of the extrapolated base line with the steepest slope of the peak was used. Melting temperatures were read at the

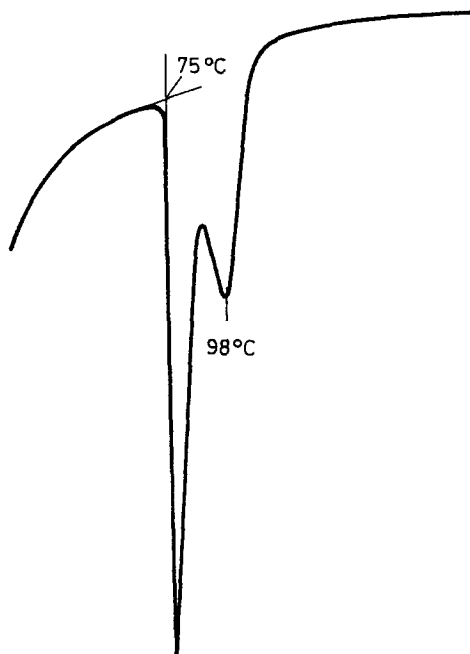


Fig. 3 Example of a DTA curve taken for the  $\text{GeI}_4$ - $\text{I}_2$  system for 12.4%  $\text{GeI}_4$

maximum of the melting peak. In Fig. 2, the composition-temperature data pairs are indicated. Temperature values of the eutectic vary around the average  $75^{\circ}$  ( $348\text{ K}$ )  $\pm 2.5^{\circ}$ . The eutectic temperature indicated in the barogram is about  $5\text{--}10^{\circ}$  higher. The calculated value also rose to the same extent. By extrapolation at 34% (n/n)  $\text{GeI}_4$ , the eutectic composition is obtained.

The curve (cf. 1. 2.) coincides with that determined by DTA.

It can be concluded from the curves determined that the particles do not interact significantly and show a nearly ideal behaviour.

No thermal effects were indicated on the cooling curves which means that a considerable supercooling took place, as it was observed for total pressure measurements over  $\text{GeI}_4\text{-I}_2$  precipitates.

Melting temperatures determined by the barogram (Fig. 1) fit into the melting behaviour determined by DTA. The liquidus lines indicated by Maneglier *et al.* [4] deviate from that determined in this paper.

## 2. The $\text{GeI}_4\text{-BiI}_3$ system

### 2.1 Total pressure measurements, barogram

Assuming ideal behaviour, an eutectic in the vicinity of the  $\text{GeI}_4$  boundary phase was expected (see 2.2.). With the mixtures, until the eutectic temperature ( $E$ ) the pressure values were measured to be along the saturation pressure line of  $\text{GeI}_4$ . The temperature of the bending point  $E$  was determined as  $143^{\circ}$  ( $416\text{ K}$ ). With further temperature increase, the pressure values measured were only slightly below the saturation curve of  $\text{GeI}_4$  (see Fig. 4). The maximum of the  $E\text{-}S_2$  three-phase line could not be exactly registered, as this range was only slightly above 760 torr and thus, beyond the measuring range. However, in realizing the experiment, it was ensured that the pressure maximum was about  $385^{\circ}$  ( $658\text{ K}$ ) and did not exceed 950 torr; (curve 2, Fig. 4). Sample 3 was mixed in such a way that in the temperature range between  $335^{\circ}$  ( $608\text{ K}$ ) and  $400^{\circ}$  ( $673\text{ K}$ ) the three-phase line was "tunnelled", i. e. the total pressure did not correspond to saturation and, only above  $400^{\circ}$ , went along the three-phase line towards  $S_2$ . The bending points to be assigned to the melting temperature were at  $403^{\circ}$  ( $676\text{ K}$ ) and 4.1% (n/n)  $\text{GeI}_4$  and  $408^{\circ}$  ( $681\text{ K}$ ) and 2.2% (n/n)  $\text{GeI}_4$ .

Total pressure measurements show that the system is single eutectic, i. e. there is neither a compound formation nor a miscibility gap. The extreme

position of the three-phase line could be explained by assuming great repulsive forces between  $\text{BiI}_3$  and  $\text{GeI}_4$ .

## 2.2 Calculation of the $\text{GeI}_4\text{-BiI}_3$ melting diagram

In calculating the liquidus line of the  $\text{BiI}_3$  boundary phase by the equation mentioned at the beginning, the following values were taken: for  $\text{BiI}_3$  the heat of fusion, 10 kcal/mol (41.9 kJ/mol) [15] and 7.6 kcal/mol (31.8 kJ/mol) [10], respectively. The molar heat difference  $\Delta C_p$  ( $\text{BiI}_3$ , liquid-solid) was estimated as 2.5 cal/k·mol (10.5 J/k·mol). This was done following the trihalide values of Barin and Knacke [8]. The melting temperature used was  $408^\circ$  (681 K).

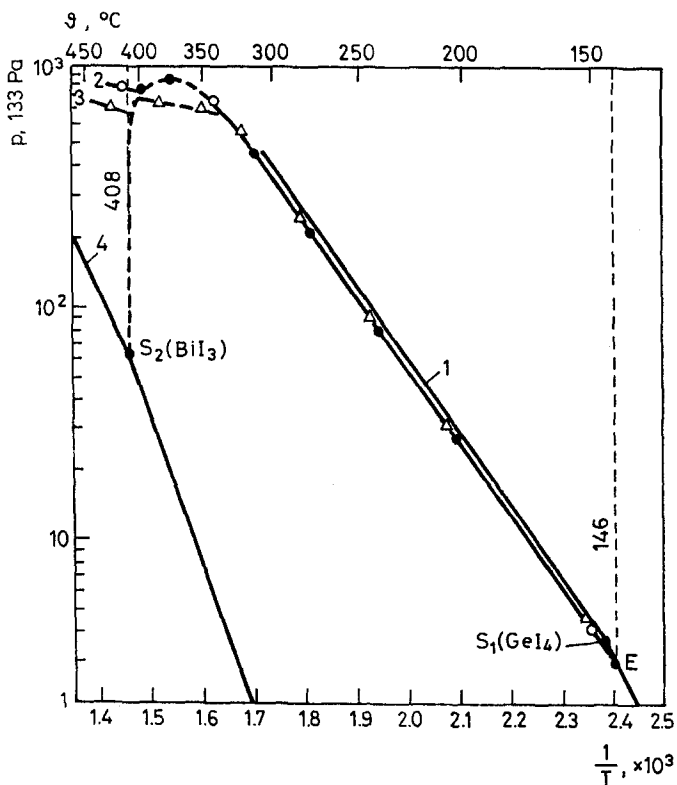


Fig. 4 Phase barogram of the  $\text{GeI}_4\text{-BiI}_3$  system Mole per cent  $\text{GeI}_4$ : 1 -  $\text{GeI}_4$ ; 2 - 4.1; 3 - 2.2; 5 -  $\text{BiI}_3$

The liquidus lines calculated in this way are shown in Fig. 5. Hence, the eutectic temperature has values which are only slightly below the melting

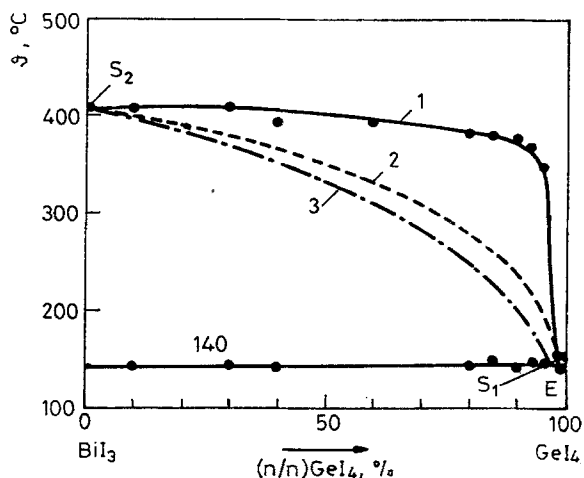


Fig. 5 Melting diagram for the system  $\text{GeI}_4\text{-BiI}_3$ ; 1 - DTA; 2 - calculated with  $\Delta H_L = 10$  kcal/mol; 3 - calculated with  $\Delta H_L = 7.67$  kcal/mol  
\* - from total pressure measurements, Fig. 4

temperature of  $\text{GeI}_4$ ; between  $140^\circ$  (413 K) and  $145^\circ$  (418 K). The eutectic would be between 1% (n/n)  $\text{GeI}_4$  and 4% (n/n)  $\text{GeI}_4$ . The various values for the heat of fusion lead to various melting temperature-molar fraction data pairs in the medium molar fraction range; with regard to the eutectic, there are nearly the same consequences.

### 2.3 Differential thermal analysis, $\text{GeI}_4\text{-BiI}_3$ melting diagram

In analogy with the previous system, weighed portions of 100 mg of the respective  $\text{GeI}_4$  and  $\text{BiI}_3$  mixtures were heated at a rate of 5 deg/min. The results are indicated in Fig. 5. The system is a single eutectic, the eutectic is at 97% (n/n)  $\text{GeI}_4$  and  $140^\circ$  (413 K)  $\pm 2.5^\circ$ . The coordinates determined by DTA for the eutectic coincide with those determined by calculation. The liquidus line determined by DTA is far beyond that determined for  $\text{BiI}_3$ . This is explained by a considerable interaction between  $\text{BiI}_3$  and  $\text{GeI}_4$  as has already been concluded from the extreme course of the three-phase line in the pressure measurements (cf. 2. 1., Fig. 4). The sharp decline of the melting curve towards the eutectic point is in agreement with the steepness of the three-phase line and the related pressure maximum in the barogram.



### 3. The GeI<sub>4</sub>-HgI<sub>2</sub> system

#### 3.1 Total pressure measurements, barogram

The phase barogram of the GeI<sub>4</sub>-HgI<sub>2</sub> system shows a special feature, e. g. both boundary phases have nearly the same vapour pressure.

To describe the phase barogram (Fig. 6), three weighed portions were selected, one on the right side of the eutectic, two on the left side of the eutectic with a high content of HgI<sub>2</sub>. Sample 2 in Fig. 6 shows a pressure course along GeI<sub>4</sub> saturation curve up to nearly 145° (418 K) and afterwards it is lower. The real solid composition at the bending point is 1% (n/n) HgI<sub>2</sub>. In the initial range, the total pressure of samples 3, 4 and 5 is lower than the GeI<sub>4</sub> saturation vapour pressure (curve 1), however, it increases more steeply and intersects the vapour pressure curve of GeI<sub>4</sub> near 175° (448 K), at about 11 torr. Until the pressure maximum of about 120 torr at 245° (518 K) is reached, the three-phase line *E-S*<sub>1</sub> goes along above the saturation vapour pressure curve (1) and afterwards, steeply declines to the melting point *S*<sub>2</sub>

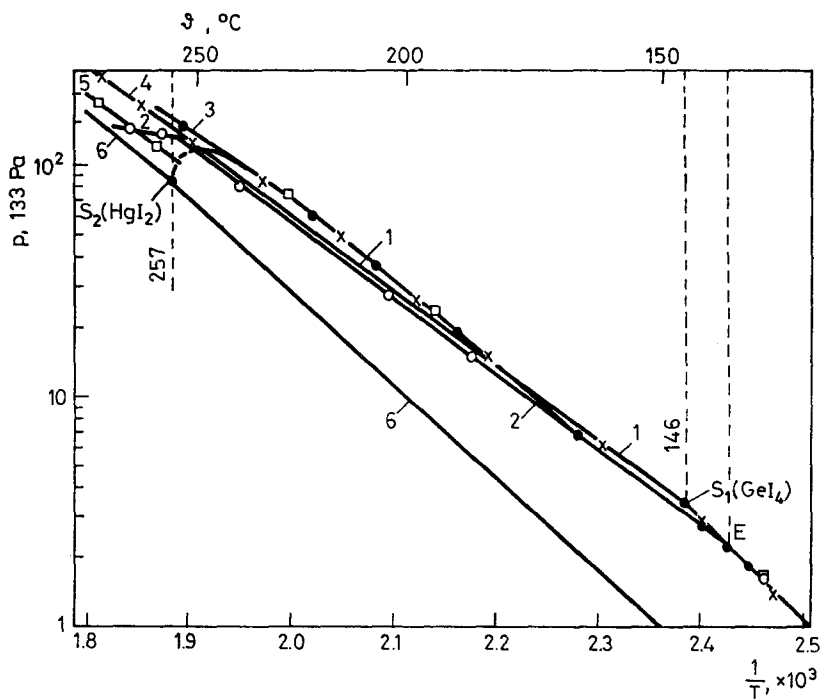


Fig. 6 Phase barogram of the GeI<sub>4</sub>-HgI<sub>2</sub> system  
Mole percent: 1 - GeI<sub>4</sub>; 2 - 99; 3 - 39; 4 - 9; 5 - 4; 6 - HgI<sub>2</sub>

of  $\text{HgI}_2$  at 80 torr (curve 5). Samples 3 and 4 leave the three-phase line at  $237^\circ$  (510 K) with 39% (n/n)  $\text{GeI}_4$  and  $248^\circ$  (521 K) and 9% (n/n)  $\text{GeI}_4$ , sample 5 at 4% (n/n)  $\text{GeI}_4$  and  $254^\circ$ .

### 3.2 Calculation of the melting diagram for $\text{GeI}_4\text{-HgI}_2$

The course of the liquidus line on the side rich in  $\text{GeI}_4$  is taken from 1. 2. To calculate the liquidus line of the side rich in  $\text{HgI}_2$ , the heat of fusion  $\Delta H_L$  equal to 4.53 kcal/mol (19 kJ/mol) [1], the molar heat difference  $\Delta C_p$  of 4.8 cal/k·mol (20.1 J/k·mol) [1, 10] and the melting temperature of  $257^\circ$  (530 K) were used; cf. [2].

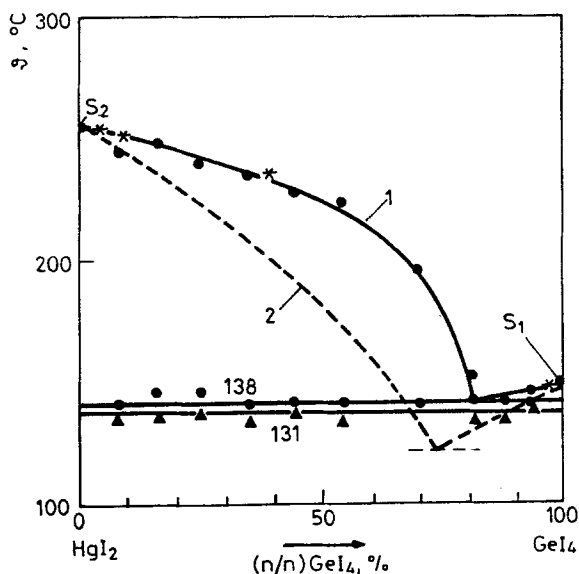


Fig. 7 Melting diagram for the  $\text{GeI}_4\text{-HgI}_2$  system; 1 - DTA; 2 - calculated with  $\Delta H_L = 4.53$  kcal/mol; \* - from total pressure measurements, Fig. 6; \*\* - limit of solubility of  $\text{GeI}_4$  in  $\text{HgI}_2$

The calculated molar fraction-temperature pairs are indicated in Fig. 7. The coordinates of the eutectic point, following these calculations, should be  $122^\circ$  (395 K) and 73% (n/n)  $\text{GeI}_4$ .

### 3.3 Differential thermal analysis, melting diagram of $\text{GeI}_4\text{-HgI}_2$

The thermal effects determined are indicated in Fig. 7. In addition to signals at the eutectic and melting point, a third signal was recorded at  $131.5^\circ$

(404 K), which is assigned to the  $\alpha$ ,  $\beta$  phase transition of  $\text{HgI}_2$  [15, 2]. By means of the behaviour determined by DTA, the eutectic temperature of  $138 \pm 2.5^\circ$  (411 K) and the eutectic composition of 82% (n/n)  $\text{GeI}_4$  can be determined. Compared with the values calculated, the experimental values are considerably higher. The behaviour of the liquidus lines determined by DTA is confirmed by the results of the total pressure measurements. Both experimentally determined liquidus lines take a course above the calculated one. Hence, it may be concluded that in this system, too, no ideal solution behaviour is observed and interactions occur.

### 3.4 Solubility of $\text{GeI}_4$ in solid $\text{HgI}_2$

With regard to the optoelectronic properties of  $\text{HgI}_2$  [16], mainly the solubility of metal iodides of other valences is of interest. To determine the solubility limit of  $\text{GeI}_4$  in  $\text{HgI}_2$ ,  $\text{HgI}_2$  crystals were thermally treated beside  $\text{GeI}_4$  as illustrated in Fig. 8. Quartz ampoules standing vertically in a two-zone furnace were exposed to a temperature gradient of  $225^\circ$  (498 K) to  $190^\circ$  (463 K) for several days. A constant amount of  $\text{HgI}_2$  was used and the quantity of  $\text{GeI}_4$  was varied. According to the limit of solubility it was expected that  $\text{GeI}_4$  dissolved in  $\text{HgI}_2$  and the excess  $\text{GeI}_4$  should remain in the gas phase or as a condensation product. The recrystallized and doped  $\text{HgI}_2$  crystals were analyzed by mass spectrometry.

For three different weighed portions of  $\text{GeI}_4$  with 50 mg and 120 mg and 500 mg  $\text{HgI}_2$  in each case a percentage of 0.04, 0.06 and 0.05 (n/n)  $\text{GeI}_4$  was

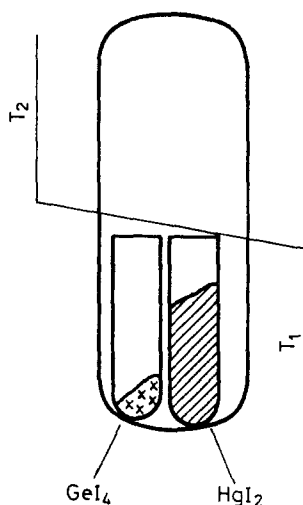


Fig. 8 Experimental arrangement to dope  $\text{HgI}_2$  with  $\text{GeI}_4$

identified in the  $\text{HgI}_2$  crystals. Hence, the limit of solubility of  $\text{GeI}_4$  in  $\text{HgI}_2$  is about  $200^\circ$  at  $0.05 \pm 0.02$  mole per cent.

#### 4. Discussion of the results

Among the three systems investigated, the  $\text{GeI}_4\text{-I}_2$  system shows a nearly ideal solution behaviour. Hence, it resembles the  $\text{HgI}_2\text{-I}_2$  [1, 2] and  $\text{BiI}_3\text{-I}_2$  [3] systems. For these systems the phase barogram is similar since iodine has a much higher volatility than  $\text{GeI}_4$ , but the three-phase line takes a flat course and has its maximum where  $\text{GeI}_4$  has a vapour pressure of only some torr. The forces of attraction of molecules are equal.

The melting diagram and the phase barogram of the  $\text{GeI}_4\text{-BiI}_3$  system deviate considerably from the ideal solution behaviour. This deviation consists in the steep course of the three-phase line, which in the initial range is nearly identical with the saturation vapour pressure curve of  $\text{GeI}_4$ . The saturation vapour pressure of  $\text{BiI}_3$  is already some torr, interaction forces are indicated, for which the relation

$$A-A \gg A-B \ll B-B$$

is valid and, which become as effective as the repulsive forces.

The  $\text{GeI}_4\text{-HgI}_2$  system is similar to the previously described system  $\text{BiI}_3\text{-GeI}_2$ , but the phase barogram of this system is of a completely different shape because the saturation pressures are more similar. The fact that the three-phase line intersects the  $\text{GeI}_4$  saturation curve at about  $175^\circ$  and 10 torr and that the maximum is only at  $250^\circ$  (523 K), where the saturation pressure of  $\text{HgI}_2$  is already 70 torr, is in accordance with the considerable deviation of the liquidus line deviating from that determined by Raoult's equation.

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**Zusammenfassung** — Durch Gesamtdruckmessungen mittels eines Membran-nullmanometers wurden Phasenbarogramme der Systeme  $\text{GeI}_4\text{-I}_2$ ,  $\text{GeI}_4\text{-BiI}_3$  und  $\text{GeI}_4\text{-HgI}_2$  ermittelt und die resultierenden Phasendiagramme mit den an Hand von DTA-Messungen erhaltenen verglichen. Alle diese Systeme besitzen einen eutektischen Punkt.